Formation of  $C_4$ -Hydrocarbons by Oxidative Methylation of Propylene with Methane over Various Metal Oxide Catalysts

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Various metal oxides were studied as a catalyst for formation of  $\mathrm{C_4}$ -hydrocarbons by the reaction between methane and propylene in the presence of oxygen.  $\mathrm{La_2O_3}$  catalysts showed high activities for the  $\mathrm{C_4}$  formation. In the case of  $\mathrm{La_2O_3}$  catalyst modified with 3 wt%  $\mathrm{Na_2O}$ , a much higher yield of  $\mathrm{C_4}$  (10.1%) was obtained.

Since Keller and Bhashin<sup>1)</sup> reported the possibility of synthesis of  $C_2$ -hydrocarbons ( $C_2H_6+C_2H_4$ ) by oxidative coupling of methane over various metal oxides, many researchers  $2^{18}$  are beginning to work in this field. Sofranko et al. have recently shown that in the case of methane-propylene in the absence of oxygen over manganese oxide on silica, butene is a primary product by way of methyl addition to propylene. However, studies concerning the oxidative methylation of some olefins, aromatics, and nitriles containing a methyl group at  $\alpha$ -position on the electron-accepting function group are not fully made. The oxidative methylation reported by Khcheyan et al. proceeds in a medium with excess methane in the presence of oxygen to give products with new C-C and C-C bonds.  $^{10}$  It is well known that metal oxides and metal oxides modified with alkali metal oxides are effective catalysts for oxidative coupling of methane. In this paper, effective metal oxide catalysts for the formation of  $C_4$ -hydrocarbons (1- $C_4$ H<sub>8</sub>, t-2- $C_4$ H<sub>8</sub>, c-2- $C_4$ H<sub>8</sub>, and 1,3- $C_4$ H<sub>6</sub>) by oxidative methylation of propylene were investigated, using a conventional flow method at atmospheric pressure.

The catalysts used here were prepared from various metal nitrates or metal carbonates, except for  $\gamma$ -Al $_2$ O $_3$  and La $_2$ O $_3$  catalysts. The catalysts supported on  $\gamma$ -Al $_2$ O $_3$  or La $_2$ O $_3$  were prepared by an impregnation method. Each catalyst was dried at 373 K and then calcined in air at 973 K for 2 h. Prior to the reaction, the pretreatment for the activation of catalyst was performed at 973 K for 0.5 h in a flow of nitrogen and oxygen, and then for 1.5 h in a stream of nitrogen alone. The reaction conditions were as follows; reaction temperature: T=923 K, partial pressure of methane: P(CH $_4$ )=88.6 kPa, partial pressure of propylene: P(C $_3$ H $_6$ )=8.44 kPa, partial pressure of oxygen: P(O $_2$ )=4.22 kPa, and W/F=4.67 g·h/mol. The products were analyzed by gas chromatography.

Table 1 shows the typical results of the reaction on various metal oxide catalysts. The yield was calculated on the basis of conversion of propylene to the each product. As is shown in Table 1, the  $La_2O_3$  catalysts are much

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Table 1. Catalytic Activity for Oxidative Methylation of Propylene at 923 Ka)

Catalyst	Conversion/%			Yield/% <sup>b)</sup>		Distribution/%				
	CH <sub>4</sub>	<sup>С</sup> 3 <sup>Н</sup> 6	02	CO <sub>2</sub> +CO	С <sub>4</sub> - н.с.	1- C <sub>4</sub> H <sub>8</sub>	t-2- C <sub>4</sub> H <sub>8</sub>	C-2- C <sub>4</sub> H <sub>8</sub>	1,3- C <sub>4</sub> H <sub>6</sub>	n- C4 <sup>H</sup> 10
Y-Al <sub>2</sub> O <sub>3</sub>	7.5	33.5	56.3	3.49	1.28	46.5	15.1	15.4	23.0	_
10wt%CuO/Y-Al <sub>2</sub> O <sub>3</sub>	12.6	32.6	65.9	5.17	0.70	30.0	23.6	28.1	18.3	-
10wt%PbO/Y-Al <sub>2</sub> O <sub>3</sub>	6.2	29.2	60.9	5.77	1.20	28.6	15.5	21.9	34.0	-
10wt%Ag <sub>2</sub> O/Y-Al <sub>2</sub> O <sub>3</sub>	4.6	32.0	52.5	4.22	1.09	22.7	18.1	20.0	39.2	-
10wt%Bi <sub>2</sub> O <sub>3</sub> /Y-Al <sub>2</sub> O <sub>3</sub>	15.0	61.5	49.5	8.12	3.21	24.4	11.9	11.9	47.7	4.1
30wt%La <sub>2</sub> O <sub>3</sub> /Y-Al <sub>2</sub> O <sub>3</sub>	18.4	34.2	57.3	4.97	2.20	33.7	14.6	11.5	40.2	-
La <sub>2</sub> O <sub>3</sub>	11.4	23.6	45.6	3.79	6.89	44.1	20.4	18.2	17.3	-
3wt%Na <sub>2</sub> O/La <sub>2</sub> O <sub>3</sub>	8.7	29.4	79.6	4.50	10.1	55.2	15.7	13.9	15.2	-
8wt%Na <sub>2</sub> O/La <sub>2</sub> O <sub>3</sub>	7.5	24.0	71.8	4.07	6.70	61.3	11.6	11.7	15.4	-

a) Data at 60 min. b) Calculated on the basis of propylene conversion; the rest was an yield of carbon deposit.

more effective for the reaction than the other catalysts. In addition, the  $\text{La}_2\text{O}_3$  catalysts modified with  $\text{Na}_2\text{O}$  in the range of 1 to 5 wt% exhibited much more activity for C<sub>4</sub> formation than the La<sub>2</sub>O<sub>3</sub> catalyst without Na<sub>2</sub>O. further addition of  $Na_2O$  over 8 wt% resulted in a decrease in the yield of  $C_4$ . On the other hand, the  $\gamma-\text{Al}_2\text{O}_3$ ,  $\text{CuO}/\gamma-\text{Al}_2\text{O}_3$ ,  $\text{PbO}/\gamma-\text{Al}_2\text{O}_3$ , and  $\text{Ag}_2\text{O}/\gamma-\text{Al}_2\text{O}_3$ catalysts were found to give remarkably lower yields of C4 than the La203 catalysts. In the cases of  $Bi_2O_3/\gamma-Al_2O_3$  and  $La_2O_3/\gamma-Al_2O_3$  catalysts, the yields of  $C_4$  were improved considerably, compared with the  $\gamma$ -Al $_2$ O $_3$  catalyst. The distribution of  $C_4$ -hydrocarbons depends on the catalyst, as can be seen from Table 1. In addition, the formation of  $\mathrm{C}_2$ -hydrocarbons was not observed in every case, because of relatively lower reaction temperature of 923 K.

The  $La_2O_3$  catalyst with 3 wt%  $Na_2O$  gave a maximum  $C_4$  yield of 10.1% and the yield remained almost constant for 2 h of reaction time, in spite of the From these facts, it can be said that developed formation of carbon deposit. studies on the oxidative methylation of propylene will be able to give much more yield of  $C_A$ -hydrocarbons than that described in this communication.

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